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ISO 9906:2012(E)

Foreword

ISO (the International Organization for Standardization) is a worldwide federation of national standards bodies (ISO member bodies). The work of preparing International Standards is normally carried out through ISO technical committees. Each member body interested in a subject for which a technical committee has been established has the right to be represented on that committee. International organizations, governmental and non-governmental, in liaison with ISO, also take part in the work. ISO collaborates closely with the International Electrotechnical Commission (IEC) on all matters of electrotechnical standardization.

International Standards are drafted in accordance with the rules given in the ISO/IEC Directives, Part 2.

The main task of technical committees is to prepare International Standards. Draft International Standards adopted by the technical committees are circulated to the member bodies for voting. Publication as an International Standard requires approval by at least 75 % of the member bodies casting a vote.

Attention is drawn to the possibility that some of the elements of this document may be the subject of patent rights. ISO shall not be held responsible for identifying any or all such patent rights.

ISO 9906 was prepared by Technical Committee ISO/TC 115, Pumps, Subcommittee SC 2, Methods of measurement and testing.

This second edition cancels and replaces the first edition (ISO 9906:1999), which has been technically revised.
Introduction

The tests in this International Standard are intended to ascertain the performance of the pump and to compare this with the manufacturer’s guarantee.

The nominated guarantee for any quantity is deemed to have been met if, where tested according to this International Standard, the measured performance falls within the tolerance specified for the particular quantity (see 4.4).
Rotodynamic pumps — Hydraulic performance acceptance tests — Grades 1, 2 and 3

1 Scope

This International Standard specifies hydraulic performance tests for customers’ acceptance of rotodynamic pumps (centrifugal, mixed flow and axial pumps, hereinafter “pumps”).

This International Standard is intended to be used for pump acceptance testing at pump test facilities, such as manufacturers’ pump test facilities or laboratories.

It can be applied to pumps of any size and to any pumped liquids which behave as clean, cold water.

This International Standard specifies three levels of acceptance:

— grades 1B, 1E and 1U with tighter tolerance;
— grades 2B and 2U with broader tolerance;
— grade 3B with even broader tolerance.

This International Standard applies either to a pump itself without any fittings or to a combination of a pump associated with all or part of its upstream and/or downstream fittings.

2 Normative references

The following referenced documents are indispensable for the application of this document. For dated references, only the edition cited applies. For undated references, the latest edition of the referenced document (including any amendments) applies.

ISO 17769-1, Liquid pumps and installation — General terms, definitions, quantities, letter symbols and units — Part 1: Liquid pumps

ISO 17769-2, Liquid pumps and installation — General terms, definitions, quantities, letter symbols and units — Part 2: Pumping system

3 Terms, definitions, symbols and subscripts

3.1 Terms and definitions

For the purposes of this document, the terms, definitions, quantities and symbols given in ISO 17769-1 and 17769-2 and the following apply.

NOTE 1 Table 1 gives an alphabetical list of the symbols used and Table 2 gives a list of subscripts; see 3.3.

NOTE 2 All formulae are given in coherent SI units. For conversion of other units to SI units, see Annex I.

3.1.1 General terms

NOTE All of the types of test in 3.1.1 apply to guarantee point to fulfil the customer’s specification(s).

3.1.1.1 guarantee point

flow/head ($Q/H$) point, which a tested pump shall meet, within the tolerances of the agreed acceptance class
3.1.1.2  
factory performance test  
pump test performed to verify the initial performance of new pumps as well as checking for repeatability of production units, accuracy of impeller trim calculations, performance with special materials, etc.  

NOTE  A typical performance test consists of the measurement of flow, head and power input to the pump or pump test motor. Additional measurements, such as NPSH, may be included as agreed upon. A factory test is understood to mean testing at a dedicated test facility, often at a pump manufacturer’s plant or at an independent pump test facility.  

3.1.1.3  
non-witnessed pump test  

3.1.1.3.1  
factory test  
test performed without the presence of a purchaser’s representative, in which the pump manufacturer is responsible for the data collection and judgement of pump acceptance  

NOTE  The advantage of this test is cost savings and accelerated pump delivery to the pump user. In many cases, if the purchaser is familiar with the performance of the pump (e.g. identical pump model order), a factory non-witnessed test may be acceptable.  

3.1.1.3.2  
signed factory test  
test performed without the presence of a purchaser’s representative, in which the pump manufacturer is responsible for compliance with the parameters of the agreed acceptance class  

NOTE  The pump manufacturer conducts the test, passes judgement of pump acceptance and produces a signed pump test document. The advantage of this test is the same as seen on the non-witnessed test. Compared to a witnessed test, this test is substantially less expensive and often leads to accelerated pump delivery to the end user.  

3.1.1.4  
worntessed pump test  

NOTE  The witnessing of a pump test by a representative of the pump purchaser can serve many useful functions. There are various ways of witnessing a test.  

3.1.1.4.1  
worntessing by the purchaser’s representative  
testing physically attended by a representative of the purchaser, who signs off on the raw test data to certify that the test is performed satisfactorily  

NOTE  It is possible for final acceptance of the pump performance to be determined by the witness. The benefit of witness testing depends largely on the effectiveness and expertise of the witness. A witness cannot only ensure the test is conducted properly, but also observes operation of the pump during testing prior to pump shipment to the job site. A disadvantage of witness testing can be extended delivery times and excessive cost. With just-in-time manufacturing methods, the scheduling of witness testing requires flexibility on the part of the witness and can lead to additional costs if the schedule of the witness causes delays in manufacturing.  

3.1.1.4.2  
remote witnessing by the purchaser’s representative  
pump performance testing witnessed from a distance by the purchaser or his/her representative  

NOTE  With a remote camera system, the purchaser can monitor the entire testing remotely in real-time. The raw data, as recorded by the data acquisition system, can be viewed and analysed during the test, and the results can be discussed and submitted for approval. The advantages of this type of testing are savings in travel costs and accelerated pump delivery.
3.2 Terms relating to quantities

3.2.1 angular velocity
\( \omega \)
number of radians of shaft rotation

NOTE 1 It is given by:
\[
\omega = 2\pi n
\] (1)

NOTE 2 It is expressed in time, e.g. s\(^{-1}\), where \( n \) is given in 60 \( \times \) min\(^{-1}\).

3.2.2 speed of rotation
number of rotations per second

3.2.3 mass flow rate
rate of flow discharged into the pipe from the outlet connection of the pump

NOTE 1 The mass flow rate is given in kilograms per second.

NOTE 2 The following losses or limiting effects are inherent to the pump:

a) discharge necessary for hydraulic balancing of axial thrust;

b) cooling of the pump bearings.

NOTE 3 Leakage from the fittings, internal leakage, etc., are not to be reckoned in the rate of flow. On the contrary, all derived flows for other purposes, such as

a) cooling of the motor bearings, and

b) cooling of a gear box (bearings, oil cooler)

are to be reckoned in the rate of flow.

NOTE 4 Whether and how these flows should be taken into account depends on the location of their derivation and of the section of flow-measurement respectively.

3.2.4 volume rate of flow
rate of flow at the outlet of the pump, given by:
\[
Q = \frac{q}{\rho}
\] (2)

NOTE In this International Standard, this symbol may also designate the volume rate of flow in any given section. It is the quotient of the mass rate of flow in this section by the density. (The section may be designated by subscripts.)

3.2.5 mean velocity
mean value of the axial speed of flow, given by:
\[
U = \frac{Q}{A}
\] (3)

NOTE Attention is drawn to the fact that in this case, \( Q \) may vary for different reasons across the circuit.

3.2.6 local velocity
speed of flow at any given point
3.2.7
head
energy of mass of liquid, divided by acceleration due to gravity, \( g \), given by:

\[
H = \frac{v}{g}
\]  

See 3.2.16.

3.2.8
reference plane
any horizontal plane used as a datum for height measurement

NOTE For practical reasons, it is preferable not to specify an imaginary reference plane.

3.2.9
height above reference plane
height of the considered point above the reference plane

See Figure A.1.

NOTE Its value is:
— positive, if the considered point is above the reference plane;
— negative, if the considered point is below the reference plane.

3.2.10
gauge pressure
pressure relative to atmospheric pressure

NOTE 1 Its value is:
— positive, if this pressure is greater than the atmospheric pressure;
— negative, if this pressure is less than the atmospheric pressure.

NOTE 2 All pressures in this International Standard are gauge pressures read from a manometer or similar pressure sensing instrument, except atmospheric pressure and the vapour pressure of the liquid, which are expressed as absolute pressures.

3.2.11
velocity head
kinetic energy of the liquid in movement, divided by \( g \), given by:

\[
\frac{U^2}{2g}
\]

3.2.12
total head
overall energy in any section

NOTE 1 The total head is given by:

\[
H_x = z_x + \frac{p_x}{\rho g} + \frac{U_x^2}{2g}
\]

where
- \( z \) is the height of the centre of the cross-section above the reference plane;
- \( p \) is the gauge pressure related to the centre of the cross-section.

NOTE 2 The absolute total head in any section is given by:
\[ H_{s(\text{abs})} = z_x + \frac{p_x}{\rho g} + \frac{p_{\text{amb}}}{\rho g} + \frac{U_x^2}{2g} \]  

(7)

3.2.13
inlet total head
overall energy at the inlet section of the pump

NOTE    Inlet total head is given by:

\[ H_1 = z_1 + \frac{p_1}{\rho g} + \frac{U_1^2}{2g} \]  

(8)

3.2.14
outlet total head
overall energy at the outlet section of the pump

NOTE    Outlet total head is given by:

\[ H_2 = z_2 + \frac{p_2}{\rho g} + \frac{U_2^2}{2g} \]  

(9)

3.2.15
pump total head
algebraic difference between the outlet total head, \( H_2 \), and the inlet total head, \( H_1 \)

NOTE 1   If compressibility is negligible, \( H = H_2 - H_1 \). If the compressibility of the pumped liquid is significant, the density, \( \rho \), should be replaced by the mean value:

\[ \rho_m = \frac{\rho_1 + \rho_2}{2} \]  

(10)

and the pump total head should be calculated by Formula (12):

\[ H = z_2 - z_1 + \frac{p_2 - p_1}{\rho_m g} + \frac{U_2^2 - U_1^2}{2g} \]  

(11)

NOTE 2   The correct mathematical symbol is \( H_{1-2} \).

3.2.16
specific energy
energy of liquid, given by:

\[ y = gH \]  

(12)

3.2.17
loss of head at inlet
difference between the total head of the liquid at the measuring point and the total head of the liquid in the inlet section of the pump

3.2.18
loss of head at outlet
difference between the total head of the liquid in the outlet section of the pump and the total head of the liquid at the measuring point

3.2.19
pipe friction loss coefficient
coefficient for the head loss by friction in the pipe